

Numerical methods

Review: models

Classifications

- Mechanistic / Statistical
- Deterministic / Stochastic
- Analytical / Computational

Reasons for computer methods (*iterative calculations*)

- Numerical integration
- Parameter estimation
- Data analysis

Reasons for modeling

- Prediction / Forecasting
- Understanding

Simulation → generate data

Data analysis → reduce amount of data

Some common problems that require numerical solutions (not exclusive list)

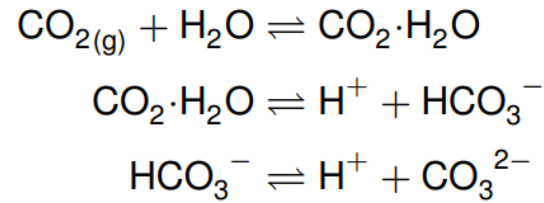
- Constraint satisfaction (solving system of equations)
- Parameter estimation (“best fit” to data)
- Numerical integration (prediction / forecasting)

Constraint satisfaction

Constraint satisfaction

- Find set of values that satisfies a system of linear or nonlinear equations (i.e., “solve” the system of equations)
- Also falls under the umbrella of AI, operations research
- The system of equations can also be a set of logical statements (“logic programming”) but this is a separate domain
- Example: phase equilibria problem

Stoichiometric balance:



Total concentration:

$$\begin{aligned}[\text{CO}_2^T] &= [\text{CO}_2 \cdot \text{H}_2\text{O}] + [\text{HCO}_3^-] + [\text{CO}_3^{2-}] \\ &= H_{\text{CO}_2} p_{\text{CO}_2} \left(1 + \frac{K_{c1}}{[\text{H}^+]} + \frac{K_{c1} K_{c2}}{[\text{H}^+]^2} \right)\end{aligned}$$

Mass law expressions:

$$\begin{aligned}K_{hc} = H_{\text{CO}_2} &= \frac{[\text{CO}_2 \cdot \text{H}_2\text{O}]}{p_{\text{CO}_2}} \\ K_{c1} &= \frac{[\text{H}^+][\text{HCO}_3^-]}{[\text{CO}_2 \cdot \text{H}_2\text{O}]} \\ K_{c2} &= \frac{[\text{H}^+][\text{CO}_3^{2-}]}{[\text{HCO}_3^-]}\end{aligned}$$

Effective Henry's law constant:

$$H_{\text{CO}_2}^* = H_{\text{CO}_2} \left(\frac{K_{c1}}{[\text{H}^+]} + \frac{K_{c1} K_{c2}}{[\text{H}^+]^2} \right)$$

Note that

$$H_{\text{CO}_2}^* > H_{\text{CO}_2}$$

Concentrations:

$$\begin{aligned}[\text{CO}_2 \cdot \text{H}_2\text{O}] &= H_{\text{CO}_2} p_{\text{CO}_2} \\ [\text{HCO}_3^-] &= \frac{K_{c1} [\text{CO}_2 \cdot \text{H}_2\text{O}]}{[\text{H}^+]} = \frac{H_{\text{CO}_2} K_{c1} p_{\text{CO}_2}}{[\text{H}^+]} \\ [\text{CO}_3^{2-}] &= \frac{K_{c2} [\text{HCO}_3^-]}{[\text{H}^+]} = \frac{H_{\text{CO}_2} K_{c1} K_{c2} p_{\text{CO}_2}}{[\text{H}^+]^2}\end{aligned}$$

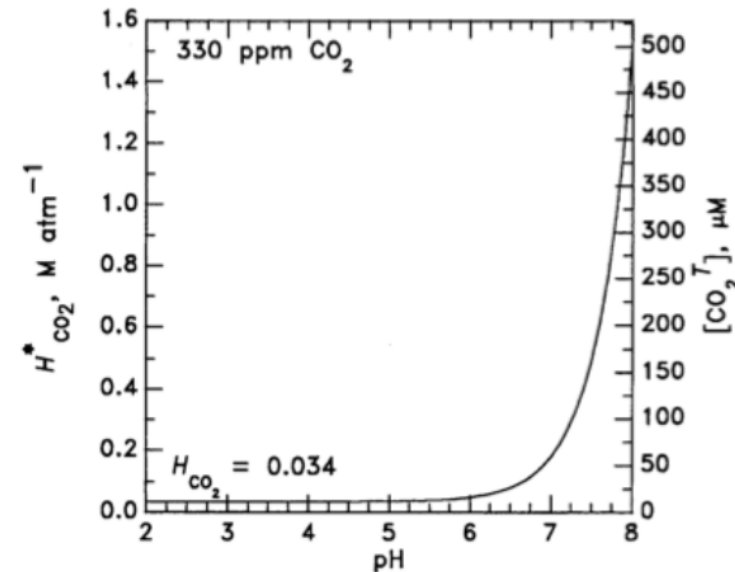


FIGURE 7.4 Effective Henry's law constant for CO_2 as a function of the solution pH. Also shown is the corresponding equilibrium total dissolved CO_2 concentration $[\text{CO}_2^T]$ for a CO_2 mixing ratio of 330 ppm.

Example: pH of “pure” rainwater

For a system containing only CO_2 with mixing ratio of $\xi_{\text{CO}_2} = 350$ ppm and water at 298 K, what is the pH of cloudwater and rain droplets in this system (assume equilibrium between gas and condensed phase)?

Charge balance

$$[\text{H}^+] = [\text{OH}^-] + [\text{HCO}_3^-] + 2[\text{CO}_3^{2-}]$$

Replace concentrations with mass law relations:

$$[\text{H}^+] = \frac{K_w}{[\text{H}^+]} + \frac{H_{\text{CO}_2} K_{c1} p_{\text{CO}_2}}{[\text{H}^+]} + \frac{H_{\text{CO}_2} K_{c1} K_{c2} p_{\text{CO}_2}}{[\text{H}^+]^2}$$

Rearrange as a cubic equation,

$$[\text{H}^+]^3 - (K_w + H_{\text{CO}_2} K_{c1} p_{\text{CO}_2}) [\text{H}^+] - 2H_{\text{CO}_2} K_{c1} K_{c2} p_{\text{CO}_2} = 0$$

$\Rightarrow$ The solution pH is 5.6.

TABLE 7.4 Thermodynamic Data for Aqueous Equilibrium Constants

Equilibrium	K at 298 K (M)	ΔH_A at 298 K, kcal mol ⁻¹
$\text{H}_2\text{O} \rightleftharpoons \text{H}^+ + \text{OH}^-$	1.0×10^{-14}	13.35
$\text{CO}_2 \cdot \text{H}_2\text{O} \rightleftharpoons \text{H}^+ + \text{HCO}_3^-$	4.3×10^{-7}	1.83
$\text{HCO}_3^- \rightleftharpoons \text{H}^+ + \text{CO}_3^{2-}$	4.7×10^{-11}	3.55
$\text{SO}_2 \cdot \text{H}_2\text{O} \rightleftharpoons \text{H}^+ + \text{HSO}_3^-$	1.3×10^{-2}	-4.16
$\text{HSO}_3^- \rightleftharpoons \text{H}^+ + \text{SO}_3^{2-}$	6.6×10^{-8}	-2.23
$\text{NH}_3 \cdot \text{H}_2\text{O} \rightleftharpoons \text{NH}_4^+ + \text{OH}^-$	1.7×10^{-5}	8.65

$$p_{\text{CO}_2} = 350 \times 10^{-9} \text{ atm}$$

$$H_{\text{CO}_2} = 3.4 \times 10^{-2} \text{ M atm}^{-1}$$

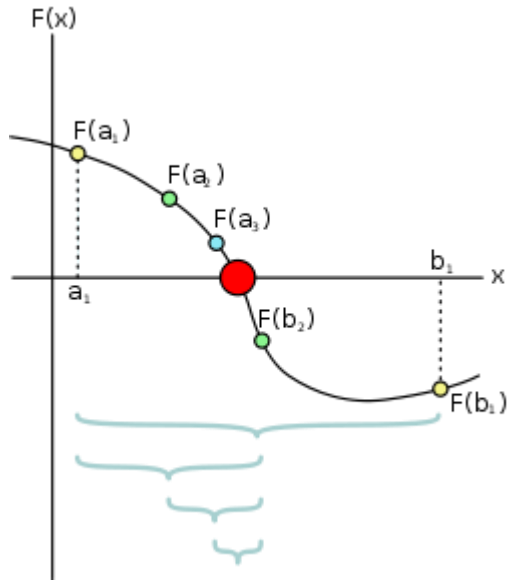
$$K_{c1} = 4.3 \times 10^{-7} \text{ M}$$

$$K_{c2} = 4.7 \times 10^{-11} \text{ M}$$

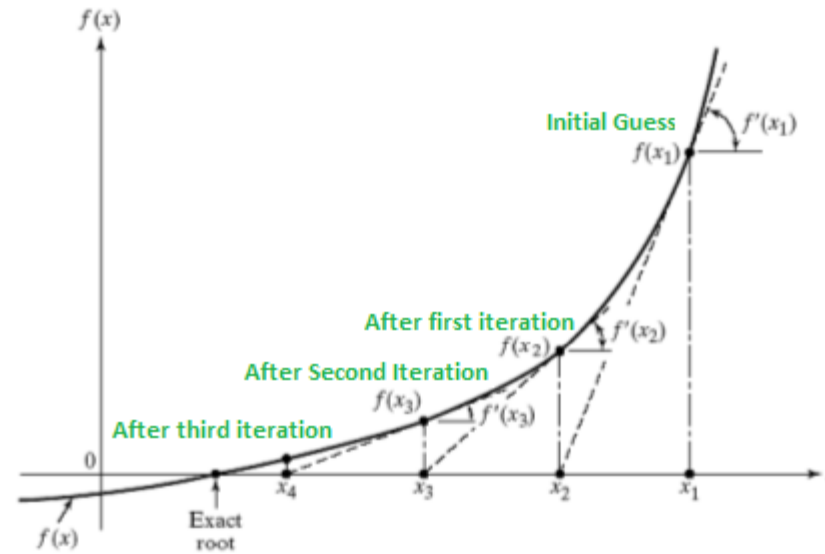
$$K_w = 10^{-14} \text{ M}$$

Simple solution methods

Bisection method



Newton-Raphson method



https://en.wikipedia.org/wiki/Bisection_method

<https://www.geeksforgeeks.org/program-for-newton-raphson-method/>

Parameter estimation

Parameter estimation

- Also falls under the umbrella of optimization, operations research, data fitting, inverse modeling, etc.
- Purposes
 - model understanding (extract physical meaning from parameter values)
 - prediction / forecasting
- Estimate parameters for empirical, semi-empirical, and mechanistic models
- Example: chemical kinetic modeling [mechanistic, nonlinear], epidemiology [semi-empirical, linear], weather prediction [empirical, nonlinear]

Example – reaction rate constants

First order reaction



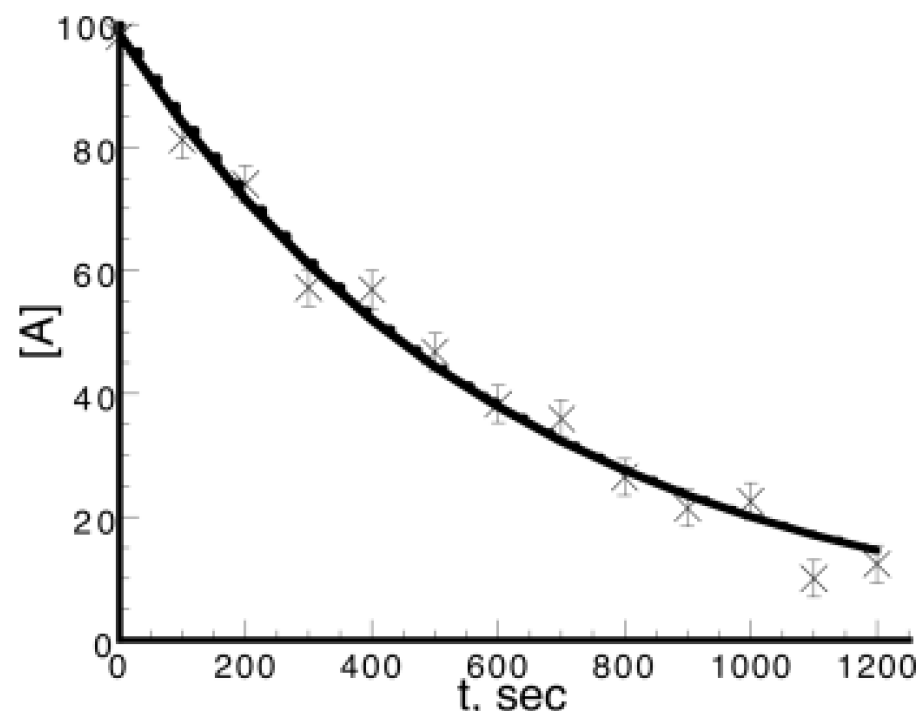
$$v = \frac{d[B]}{dt} = -\frac{d[A]}{dt} = k[A]$$

Solution to diff. eq. (estimate k to data)

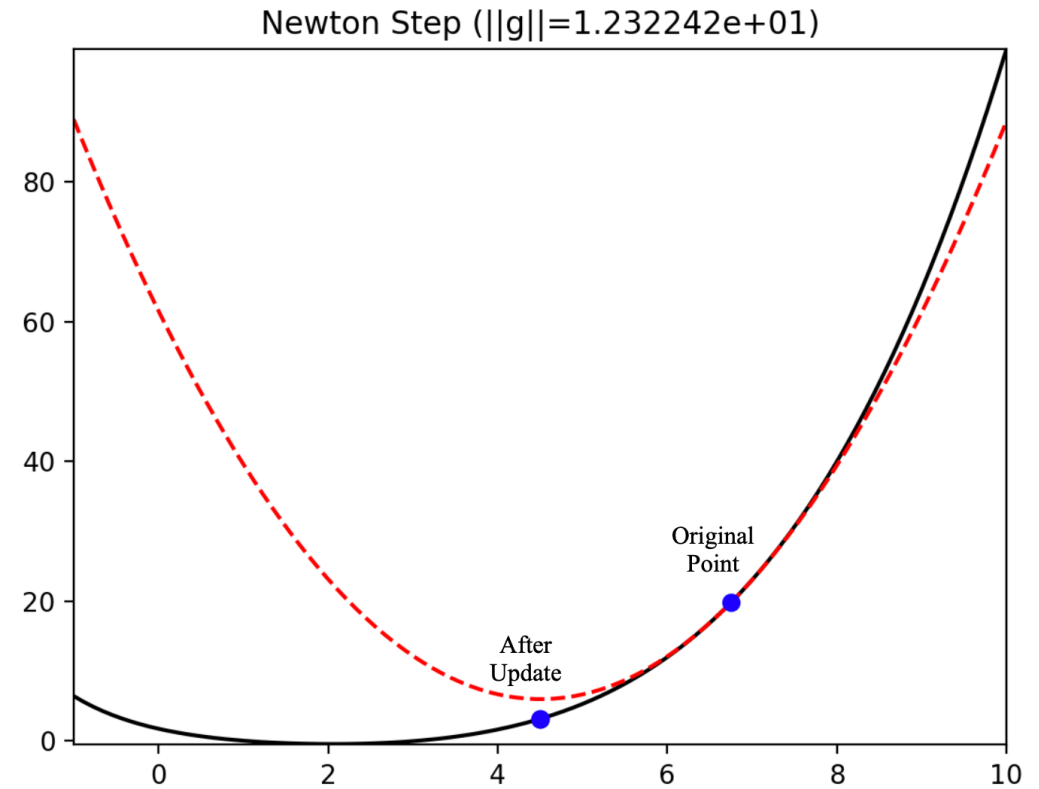
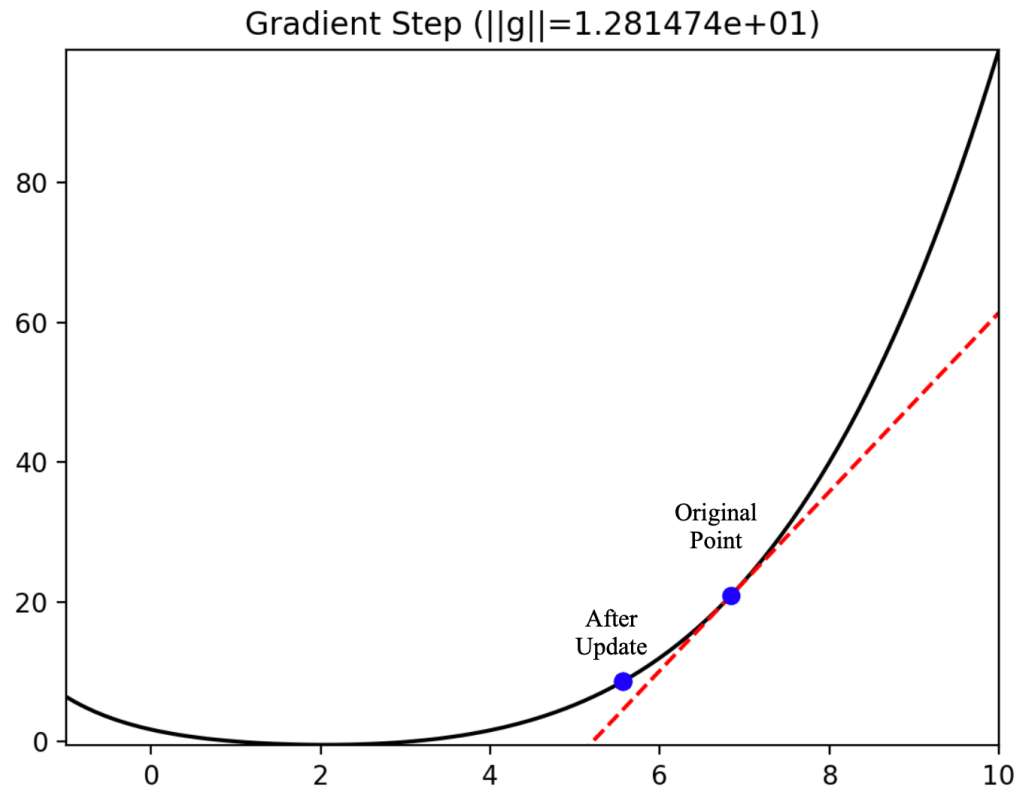
$$[A] = [A]_0 e^{-kt}$$

Objective / cost / loss function

$$J(k) = \arg \min_k \sum_i \{[\log([A]_0) - kt_i] - \log([A]_{\text{obs},i})\}^2$$



Some solution methods



Example of measurements
used for deriving rate
coefficients:

OH + NO₂ to products
 $k = k(P, T)$

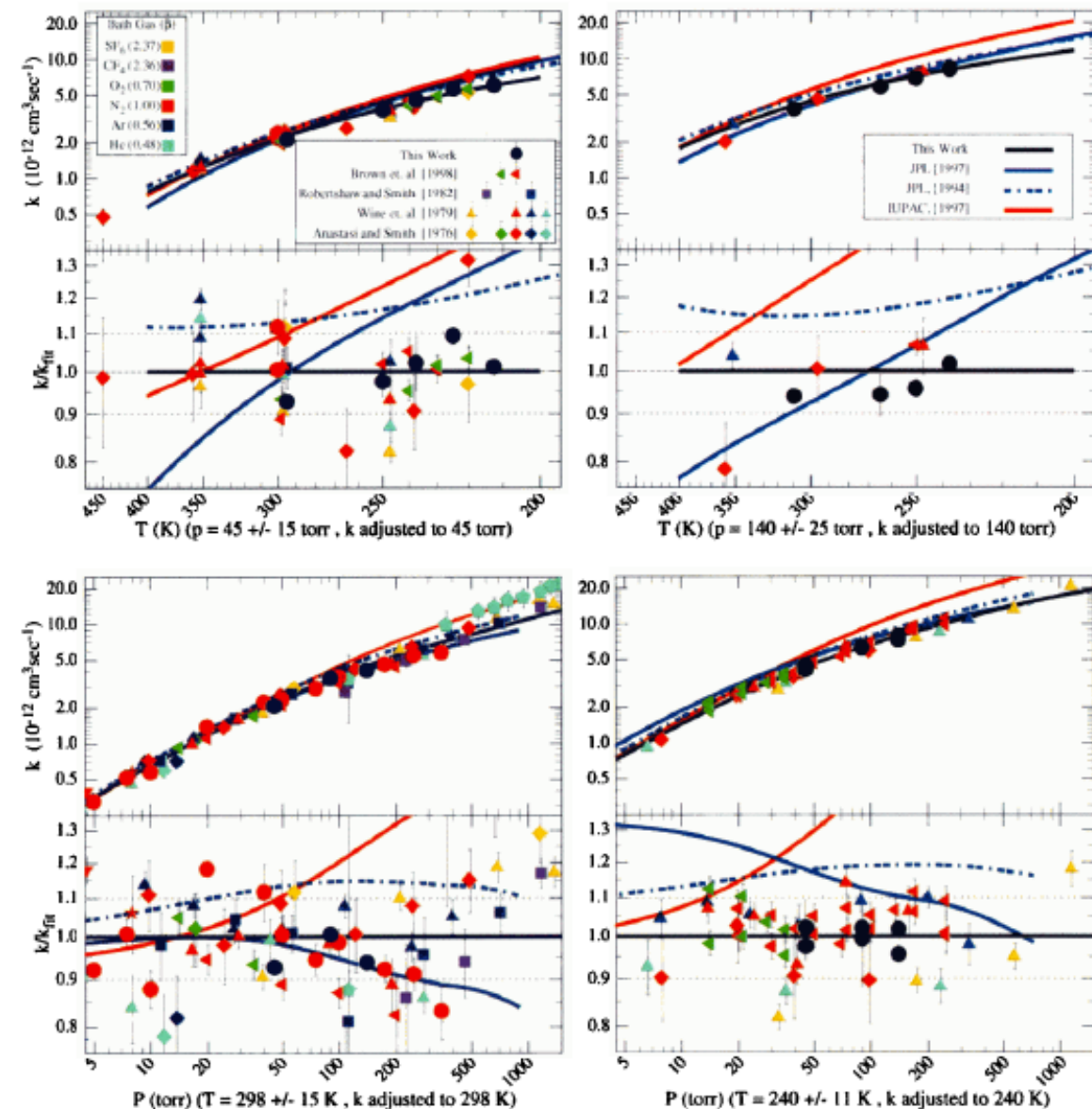


Figure 1. Data for the reaction OH + NO₂ → products as a function of pressure and temperature. Our data are plotted as solid black dots. Literature data are also shown, with different carrier gases represented by differing symbol colors. Symbol shapes identify the study responsible for each datum, as shown in the legend; the red symbol color indicates nitrogen carrier gas (with the exception of our data, which are shown as solid black for emphasis). Pressures for bath gases other than N₂ are scaled by the collisional efficiency indicated in the legend. The latest IUPAC and JPL recommendations are shown as dashed curves of the same color. Our recommendation is shown as a black curve. The lower panel of each graph shows the ratio of each value to our recommendation.



Parameters from various reactions are tabulated in a comprehensive database

Chemical Kinetics and Photochemical Data for Use in Atmospheric Studies

Evaluation Number 17

NASA Panel for Data Evaluation:

*S. P. Sander
R. R. Friedl
NASA/Jet Propulsion Laboratory*

*J. R. Barker
University of Michigan*

*D. M. Golden
Stanford University*

*M. J. Kurylo
Goddard Earth Sciences, Technology and
Research Program*

*P. H. Wine
Georgia Institute of Technology*

National Aeronautics and
Space Administration

Jet Propulsion Laboratory
California Institute of Technology
Pasadena, California

*J. P. D. Abbatt
University of Toronto*

*J. B. Burkholder
NOAA Earth System Research Laboratory*

*C. E. Kolb
Aerodyne Research, Inc.*

*G. K. Moortgat
Max-Planck Institute for Chemistry*

*R. E. Huie
V. L. Orkin
National Institute of Standards and
Technology*

<http://jpldataeval.jpl.nasa.gov/>

Table 2-1. Rate Constants for Termolecular Reactions

Reaction	Low-Pressure Limit ^a $k_L(T) = k_{L,300} (T/300)^{-n}$		High-Pressure Limit ^b $k_H(T) = k_{H,300} (T/300)^{-m}$		f	g	Notes
	$k_{L,300}$	n	$k_{H,300}$	m			
O_x Reactions							
$O + O_2 \xrightarrow{M} O_3$	(6.0) (-34)	2.4	—	—	1.1	50	A1
O('D) Reactions							
$O('D) + N_2 \xrightarrow{M} N_2O$	(2.8) (-36)	0.9	—	—	1.3	75	A2
HO_x Reactions							
$H + O_2 \xrightarrow{M} HO_2$	(4.4) (-32)	1.3	(7.5) (-11)	-0.2	1.3	50	B1
$OH + OH \xrightarrow{M} H_2O_2$	(6.9) (-31)	1.0	(2.6) (-11)	0	1.5	100	B2
NO_x Reactions							
$O + NO \xrightarrow{M} NO_2$	(9.0) (-32)	1.5	(3.0) (-11)	0.0	1.2	100	C1
$O + NO_2 \xrightarrow{M} NO_3$	(2.5) (-31)	1.8	(2.2) (-11)	0.7	1.3	100	C2
$OH + NO \xrightarrow{M} HONO$	(7.0) (-31)	2.6	(3.6) (-11)	0.1	1.2	50	C3
$OH + NO_2 \xrightarrow{M} HONO_2$	(1.8) (-30)	3.0	(2.8) (-11)	0	1.3	100	C4
$OH + NO_2 \xrightarrow{M} HOONO$	(9.1) (-32)	3.9	(4.2) (-11)	0.5	1.5	200	C4
$HO_2 + NO \xrightarrow{M} HONO_2$	See Note						C5
$HO_2 + NO_2 \xrightarrow{M} HO_2NO_2$	(2.0) (-31)	3.4	(2.9) (-12)	1.1	1.1	50	C6
$NO_2 + NO_3 \xrightarrow{M} N_2O_5$	(2.0) (-30)	4.4	(1.4) (-12)	0.7	1.2	100	C7
$NO_3 \xrightarrow{M} NO + O_2$	See Note						C8

Formerly known as:
*Chemical Kinetics and
Photochemical Data for
Use in Stratospheric
Modeling*

Chemical kinetic models are then integrated into chemical transport models which combine them with emissions, meteorology, and transport

The concentration of species i is a function of space and time: $c_i = c_i(\mathbf{r}, t)$.

$$\begin{aligned} \frac{\partial c_i}{\partial t} = & \left[\frac{\partial c_i}{\partial t} \right]_{\text{advection}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{dispersion}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{gas-phase chemistry}} \\ & + \left[\frac{\partial c_i}{\partial t} \right]_{\text{emission}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{wet/dry deposition}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{aerosol}} \\ & + \left[\frac{\partial c_i}{\partial t} \right]_{\text{aqueous-phase chemistry}} \end{aligned}$$

Mass vs. number conservation for aerosols:

- mass is important for PM_{2.5} and PM₁₀ regulation, light scattering, and mass budget considerations.
- number is important for simulating new particle formation and aerosol-cloud interactions.



FIGURE 25.1 Elements of a mathematical atmospheric chemical transport model.

Example: parameter estimation for epidemiology



ARTICLE

<https://doi.org/10.1038/s41467-021-27484-1>

OPEN

Secondary organic aerosol association with cardiorespiratory disease mortality in the United States

Havala O. T. Pye¹, Cavin K. Ward-Caviness², Ben N. Murphy¹, K. Wyatt Appel¹ & Karl M. Seltzer³

Check for updates

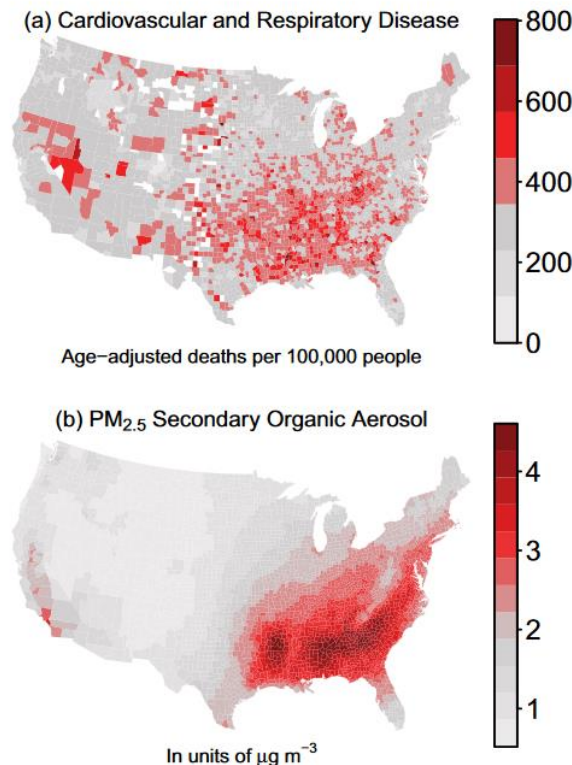
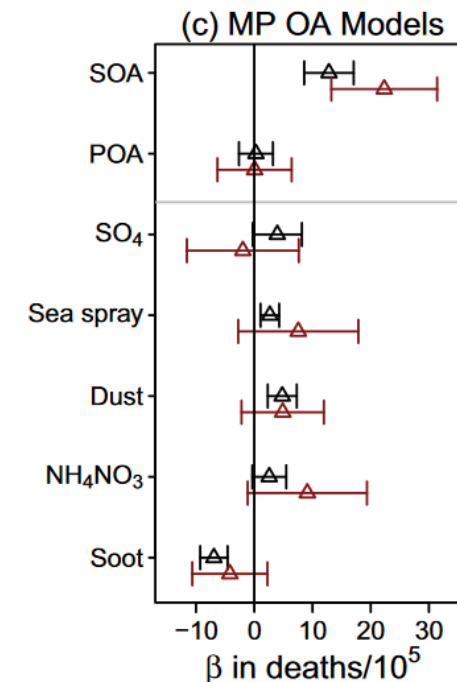


Fig. 1 Cardiorespiratory disease mortality rates and secondary organic aerosol concentrations. County-level, year 2016 (a) cardiovascular and respiratory disease age-adjusted death rates (per 100,000 in population) are from CDC and (b) PM_{2.5} secondary organic aerosol concentrations are predicted by CMAQ. White in (a) indicates no death rate data while light gray indicates low reported rates.

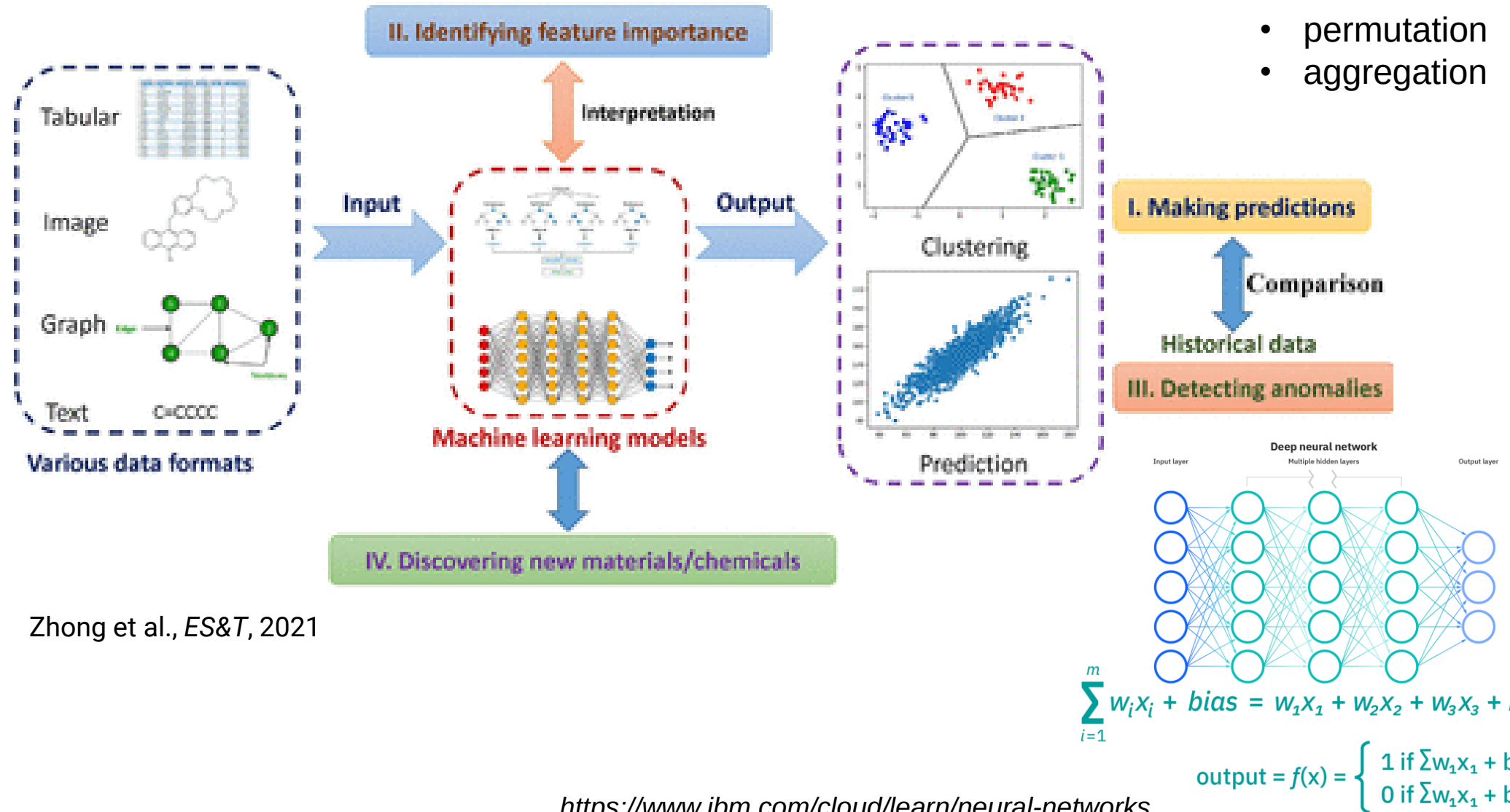
$$D = \beta_0 + \{\beta_1 PM_{SOA_{BVOC}} + \beta_2 PM_{SOA_{AVOC}} + \beta_3 PM_{POA}\} + \beta_4 PM_{Seaspray} + \beta_5 PM_{Soot} + \beta_6 PM_{NH_4NO_3} + \beta_7 PM_{SO_4} + \beta_8 PM_{Dust} + \sum_{j=1}^N \beta'_j C_j$$



Example: empirical models

Data preparation:

- cleaning
- curation
- permutation
- aggregation

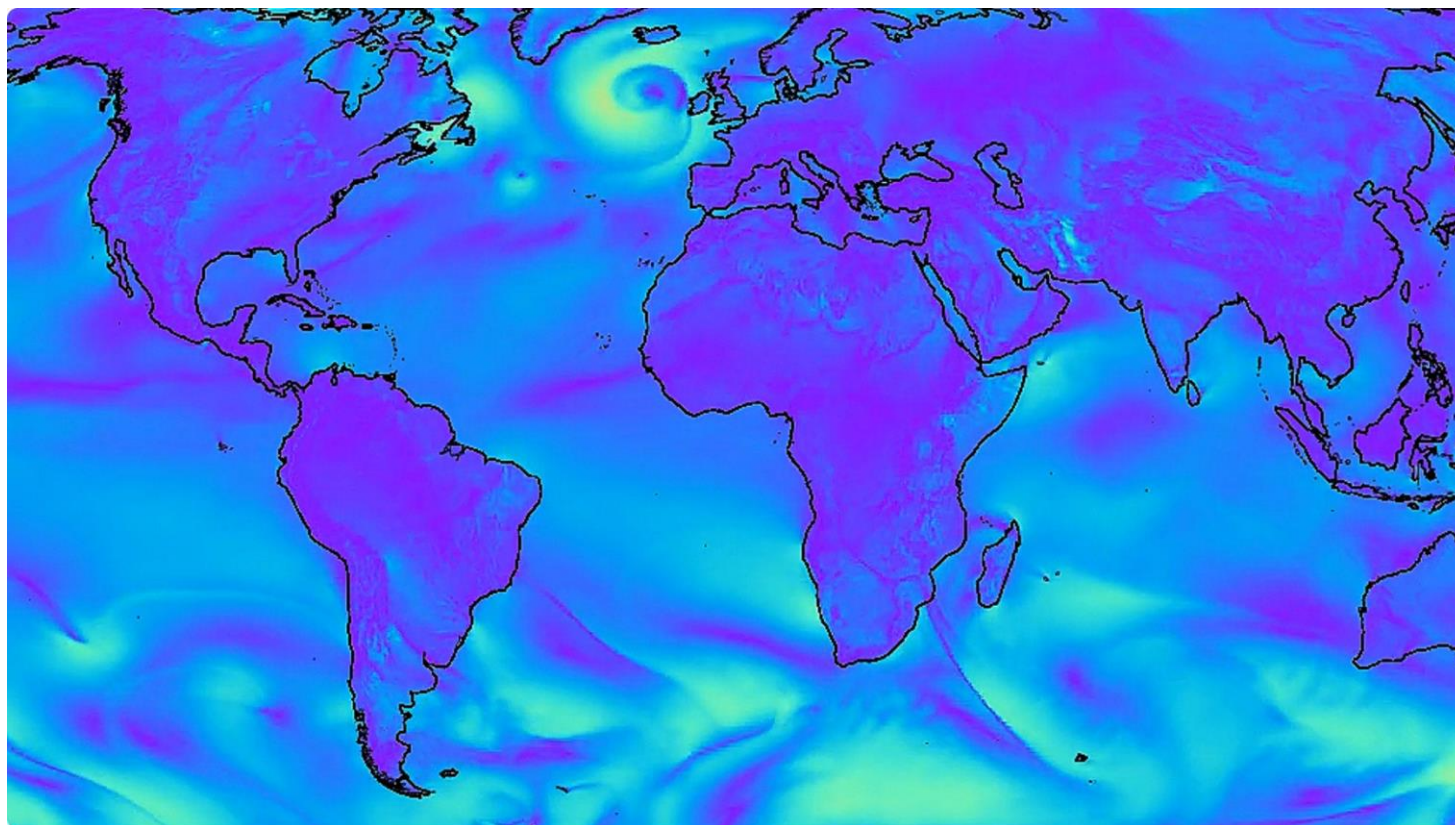
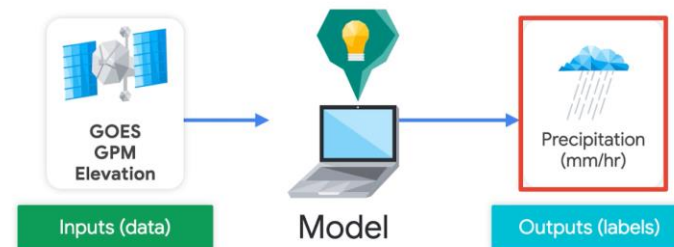


Zhong et al., *ES&T*, 2021

GREGORY BARBER BUSINESS NOV 14, 2023 10:00 AM

Google DeepMind's AI Weather Forecaster Handily Beats a Global Standard

Machine learning algorithms that digested decades of weather data were able to forecast 90 percent of atmospheric measures more accurately than Europe's top weather center.



“Gotchas”

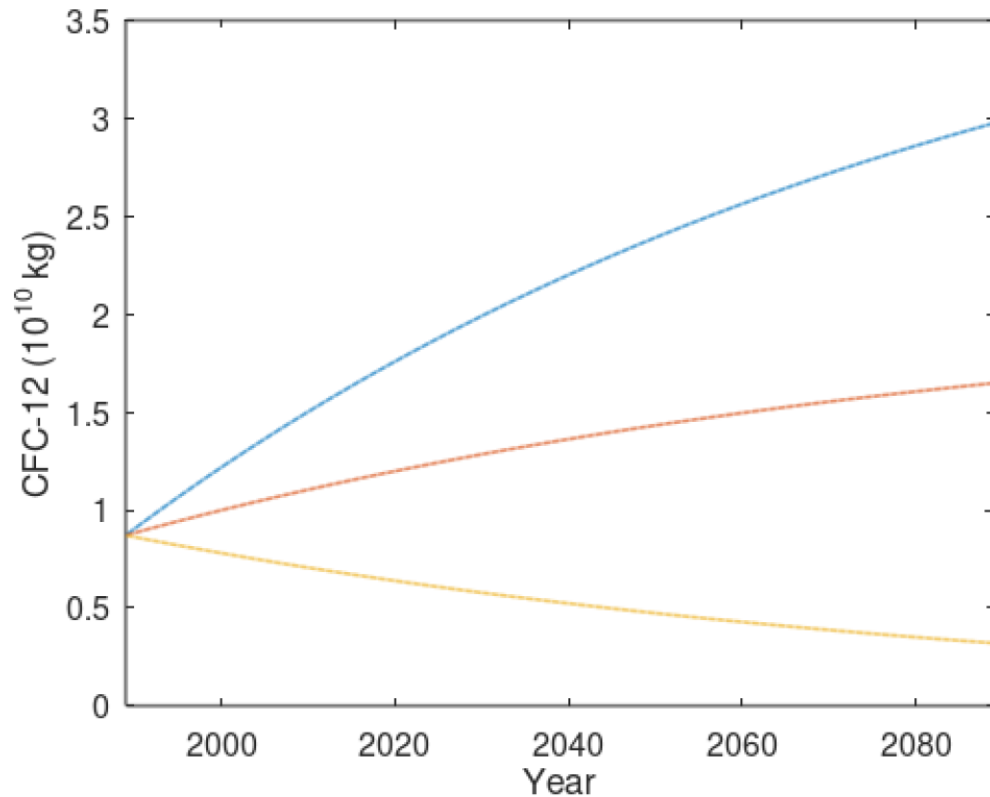
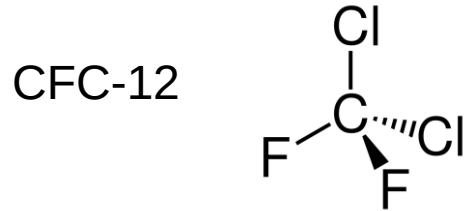
- Your estimated parameters may not be meaningful if your model (relationship among variables) is misspecified.
- Even if your model is “correct”, you may find solutions that represent local minima.
- Your predictions may not be meaningful if you are extrapolating outside of the domain of fitted data with an empirical function.

Numerical integration

Numerical integration

- Differential equation(s)
 - ODE: ordinary differential equation
 - PDE: partial differential equation
- Single, coupled, uncoupled
- Provide initial values / boundary values
- Examples: simulation of CFC-12 [single ODE], VOC-NO_x-O₃ system (urban smog) [coupled ODEs], 3D advection equation [PDE decoupled to independent ODEs]

Example (ODE): simulation of dichlorofluoromethane



The mass balance for the photolysis of CFC-12 is given by:

$$\frac{dm}{dt} = E - k m$$

m is the atmospheric mass of CFC-12, E is the rate of emission, and k is the rate of photolysis.

The atmospheric lifetime of CFC-12 is 100 years. Starting from an initial concentration of $m_0 = 400$ pptv in 1989, assume two scenarios:

"business as usual": $E = 4.2 \times 10^8$ kg/yr

Scenario 1: base case (no change)

Scenario 2: 50% reduction in emissions

Scenario 3: 50% reduction in emissions before 1996
100% reductions afterward

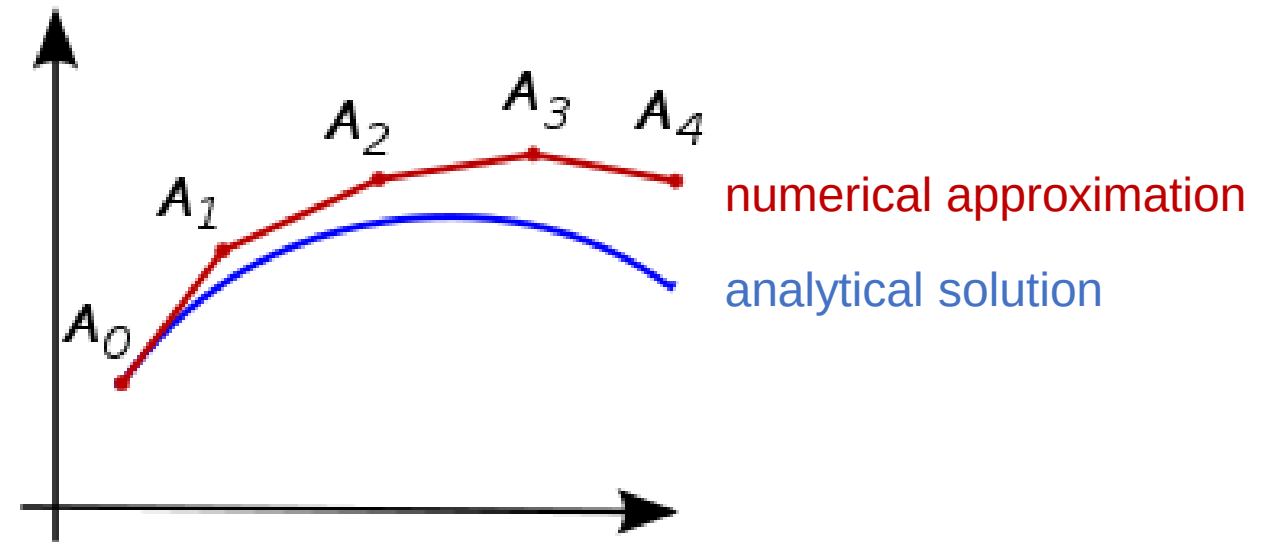
Numerical integration

Euler's method

$$y_{n+1} = y_n + h f(t_n, y_n)$$

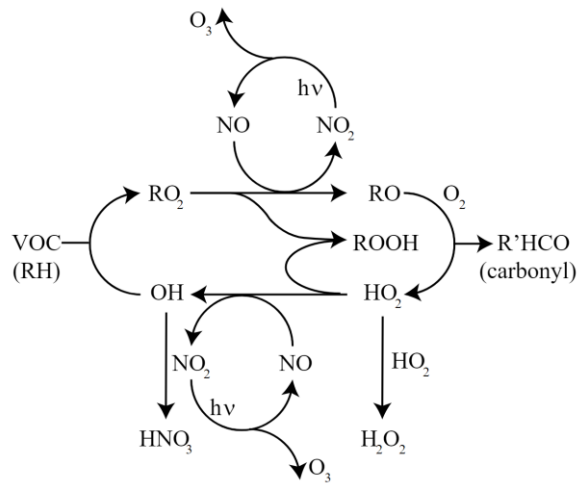
step size

derivative



https://en.wikipedia.org/wiki/Euler_method

Example (coupled ODEs): VOC-NO_x-O₃ system

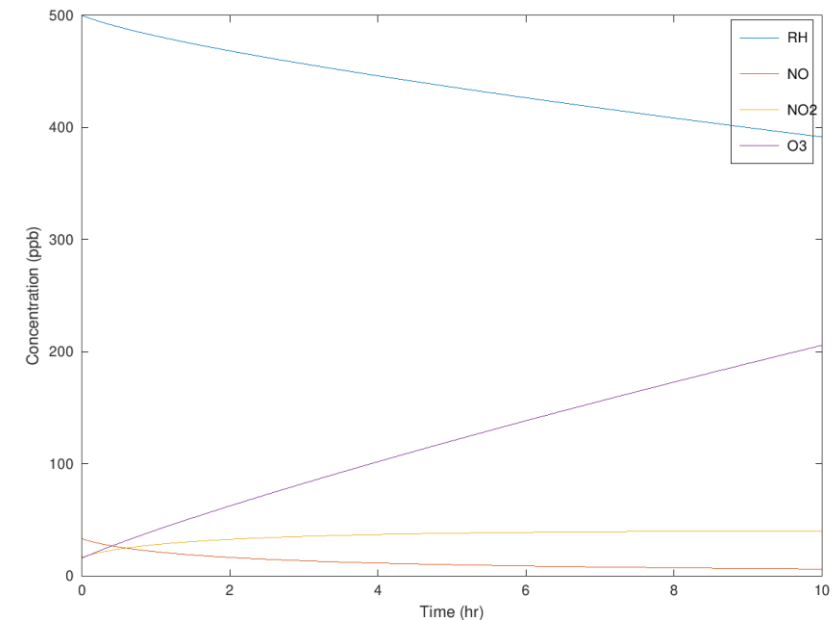


x = concentration
 ν = stoichiometric number
 r = reaction rate
 k = reaction rate constant

$$\frac{d\mathbf{x}}{dt} = \boldsymbol{\nu} \mathbf{r} = \mathbf{f}(\mathbf{x}, \mathbf{k}, \boldsymbol{\nu}), \quad \mathbf{x}(t=0) = \mathbf{x}_0$$

$$\frac{dx_i}{dt} = \sum_{j \in \text{reactions}} \nu_{ji} r_j, \quad \text{where } r_j = k_j \prod_{i \in \text{reactants}} x_i^{\nu_{ji}}$$

Reaction	Rate constant (298 K)
1 $\text{RH} + \text{OH} \xrightarrow{\text{O}_2} \text{RO}_2 + \text{H}_2\text{O}$	$26.3 \times 10^{-12} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$
2 $\text{RO}_2 + \text{NO} \xrightarrow{\text{O}_2} \text{NO}_2 + \text{R}'\text{CHO} + \text{HO}_2$	$7.7 \times 10^{-12} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$
3 $\text{HO}_2 + \text{NO} \rightarrow \text{NO}_2 + \text{OH}$	$8.1 \times 10^{-12} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$
4 $\text{OH} + \text{NO}_2 \xrightarrow{\text{M}} \text{HNO}_3$	$1.1 \times 10^{-11} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1} (\text{at } 1 \text{ atm})$
5 $\text{HO}_2 + \text{HO}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2$	$2.9 \times 10^{-12} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$
6 $\text{RO}_2 + \text{HO}_2 \rightarrow \text{ROOH} + \text{O}_2$	$5.2 \times 10^{-12} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$
7 $\text{NO}_2 + h\nu \xrightarrow{\text{O}_2} \text{NO} + \text{O}_3$	typical $\approx 0.015 \text{s}^{-1}$
8 $\text{O}_3 + \text{NO} \rightarrow \text{NO}_2 + \text{O}_2$	$1.9 \times 10^{-14} \text{cm}^3 \text{molec}^{-1} \text{s}^{-1}$



Numerical integration of PDEs

- Representation by operator splitting (requires small time steps)
- Discretization
- Finite difference
- Integration

Example: integrated modeling of multiple processes

Processes

The concentration of species i is a function of space and time: $c_i = c_i(\mathbf{r}, t)$.

$$\begin{aligned} \frac{\partial c_i}{\partial t} = & \left[\frac{\partial c_i}{\partial t} \right]_{\text{advection}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{dispersion}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{gas-phase chemistry}} \\ & + \left[\frac{\partial c_i}{\partial t} \right]_{\text{emission}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{wet/dry deposition}} + \left[\frac{\partial c_i}{\partial t} \right]_{\text{aerosol}} \\ & + \left[\frac{\partial c_i}{\partial t} \right]_{\text{aqueous-phase chemistry}} \end{aligned}$$

Mass vs. number conservation for aerosols:

- mass is important for PM_{2.5} and PM₁₀ regulation, light scattering, and mass budget considerations.
- number is important for simulating new particle formation and aerosol-cloud interactions.



FIGURE 25.1 Elements of a mathematical atmospheric chemical transport model.

Operator splitting

Let $\mathbf{c}(t) = c(\mathbf{r}, t)$. We can define an operator $X = X(\Delta t)$ and its corresponding incremental operator ΔX :

$$X \mathbf{c}(t) = [\mathbf{c}(t + \Delta t)]_X = \mathbf{c}(t) + \int_t^{t+\Delta t} \left[\frac{\partial \mathbf{c}}{\partial \tau} \right] d\tau$$

$$\Delta X \mathbf{c}(t) = [\mathbf{c}(t + \Delta t) - \mathbf{c}(t)]_X = \int_t^{t+\Delta t} \left[\frac{\partial \mathbf{c}}{\partial \tau} \right] d\tau$$

Let X represent various processes:

A Advection

D Diffusion

C Cloud

G Gas-phase chemistry

P Aerosol

S Source/sink

Operators can be applied in sequence or in parallel.

Sequential operation:

$$\mathbf{c}(t + \Delta t) = (S \circ P \circ G \circ C \circ D \circ A) \mathbf{c}(t)$$

where $\circ$ denotes operator composition: $f(g(x)) = (f \circ g)(x)$.

Parallel operation:

$$\mathbf{c}(t + \Delta t) = \mathbf{c}(t) + (\Delta S + \Delta P + \Delta G + \Delta C + \Delta D + \Delta A) \mathbf{c}(t)$$

Example: advection equation

Operator splitting is also used to decouple the processes in space. Reverting back to representation of concentration as $c = c(\mathbf{r}, t)$, consider the advection equation:

$$\frac{\partial c}{\partial t} + \mathbf{u} \cdot \nabla c = 0$$

In Cartesian coordinates,

$$\frac{\partial c}{\partial t} = -u \frac{\partial c}{\partial x} - v \frac{\partial c}{\partial y} - w \frac{\partial c}{\partial z}$$

Applying the operators in parallel,

$$c(t + \Delta t) = c(t) + \left(\Delta A_x + \Delta A_y + \Delta A_z \right) c(t)$$

we can solve three one-dimensional equations instead of one three-dimensional equation:

$$\left[\frac{\partial c}{\partial t} \right]_x = -u \frac{\partial c}{\partial x}, \quad \left[\frac{\partial c}{\partial t} \right]_y = -v \frac{\partial c}{\partial y}, \quad \text{and} \quad \left[\frac{\partial c}{\partial t} \right]_z = -w \frac{\partial c}{\partial z}$$

Discretization. Discretizing the domain and defining the concentrations over this new domain,

$$c_{i,j,k}^n = c(x_i, y_j, z_k, t_n)$$

$$c_{i,j,k}^{n+1} = c(x_i, y_j, z_k, t_n + \Delta t)$$

Representation by finite difference. We can approximate with the simplest of (backward) finite difference approximations as

$$\frac{c_{i,j,k}^{n+1} - c_{i,j,k}^n}{\Delta t} = - \frac{u_{i,j,k}^n c_{i,j,k}^n - u_{i-1,j,k}^n c_{i-1,j,k}^n}{\Delta x}$$

$$\frac{c_{i,j,k}^{n+1} - c_{i,j,k}^n}{\Delta t} = - \frac{v_{i,j,k}^n c_{i,j,k}^n - v_{i,j-1,k}^n c_{i,j-1,k}^n}{\Delta y}$$

$$\frac{c_{i,j,k}^{n+1} - c_{i,j,k}^n}{\Delta t} = - \frac{w_{i,j,k}^n c_{i,j,k}^n - w_{i,j,k-1}^n c_{i,j,k-1}^n}{\Delta z}$$

Integration (by Euler's method). We get the solution with respect to advection as

$$\begin{aligned} c_{i,j,k}^{n+1} = c_{i,j,k}^n &+ \frac{u_{i-1,j,k}^n c_{i-1,j,k}^n - u_{i,j,k}^n c_{i,j,k}^n}{\Delta x} \Delta t \\ &+ \frac{v_{i,j-1,k}^n c_{i,j-1,k}^n - v_{i,j,k}^n c_{i,j,k}^n}{\Delta y} \Delta t \\ &+ \frac{w_{i,j,k-1}^n c_{i,j,k-1}^n - w_{i,j,k}^n c_{i,j,k}^n}{\Delta z} \Delta t \end{aligned}$$

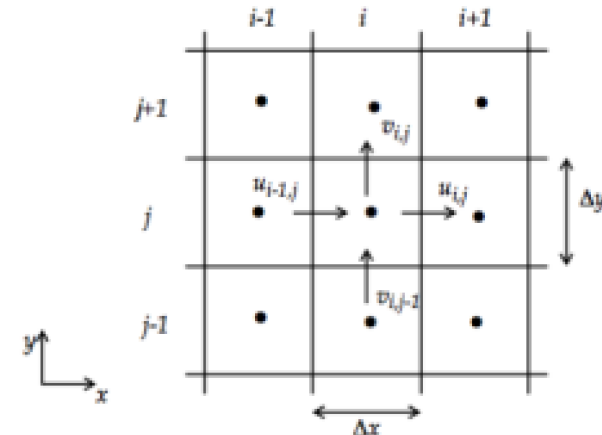
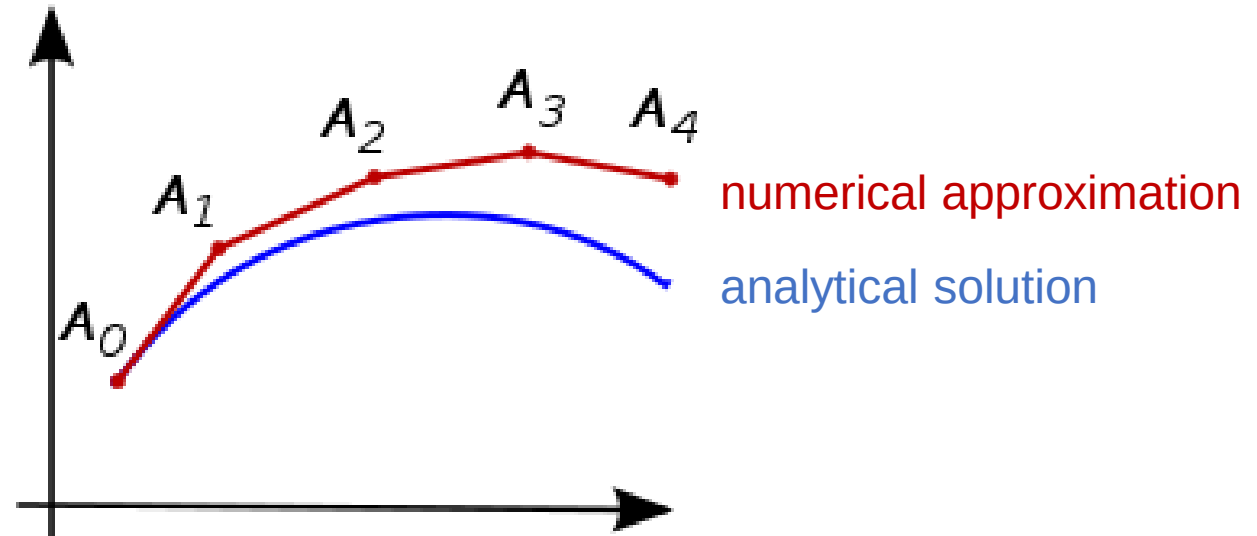


Figure 5-2 Spatial discretization of the continuity equation (only two dimensions are shown). Dots indicate gridpoints at which the concentrations are calculated, and lines indicate gridbox boundaries at which the transport fluxes are calculated.

“Gotchas”

- Your numerical approximation may not be meaningful if you pick the wrong (i.e., too large) step size (see [stiff equations](#))
- Step size should be smaller than the timescale / spatial scale of phenomena your model describes



For your project

- Many of these solvers, optimization algorithms, and numerical integration schemes are available in libraries.
- If other computational aspects of your project is high, then you can use these libraries.
- If other computation aspects of your project is low, then you can implement (i.e., code) your own version of these algorithms.

Resources for further reading

- Chapra, Steven C. and Canale, Raymond P. *Numerical Methods for Engineers*, 8th ed. McGraw-Hill Education, 2021.
- Beer, Kenneth J. *Numerical Methods for Chemical Engineering: Applications in MATLAB*, Cambridge University Press, 2007.
- Ramaswami, Anu, Milford, Jana B., Small, Mitchell J. *Integrated Environmental Modeling: Pollutant Transport, Fate, and Risk in the Environment*. John Wiley & Sons, 2005.
- Jacob, Daniel. *Introduction to Atmospheric Chemistry*. Princeton University Press, 1999. Available online: <http://acmg.seas.harvard.edu/people/faculty/djj/book/>.

Practical references for implementation

- <https://ch.mathworks.com/help/symbolic/solve-equations-numerically.html>
- <https://ch.mathworks.com/discovery/data-fitting.html>
- <https://ch.mathworks.com/help/matlab/numerical-integration-and-differentiation.html>